



Population models of turbulent heat and mass transfer

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Sept 14-18,
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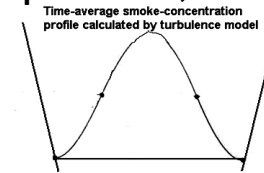
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Summary

Conventional turbulence models handle only **macro-mixing**.

They calculate the **time-mean** concentrations in plumes, arriving at skimpy, reality-missing results

e.g. for the '**profile**' across the plume like this->



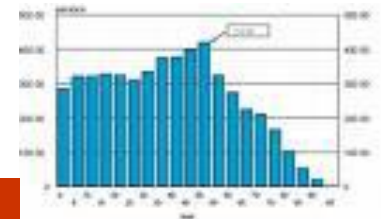
Population models of turbulence handle **micro-mixing in addition**.

They are **needed** for **realistic** prediction of **non-linear** processes such as:

- * thermal **radiation**,
- * chemical **reaction**,
- * **biological** response,
- * **fluid-structure** interaction,
- * **condensation** and evaporation,
- * **etcetera**.

Population models of turbulence predict **probability-density functions**.

They **discretize** these **pdfs**. Then they treat the histogram ordinates as dependent variables of individual **conservation equations**.



'They also allow **population-grid refinement**'.

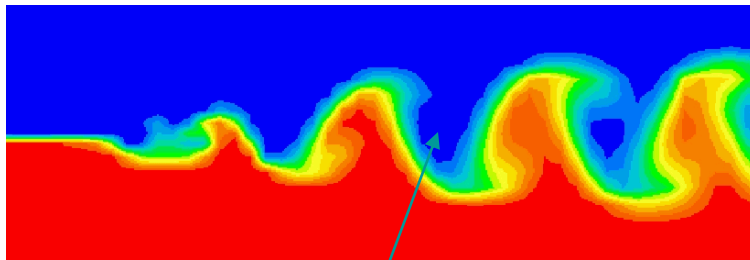


Population models of turbulent heat and mass transfer; how turbulent mixing proceeds

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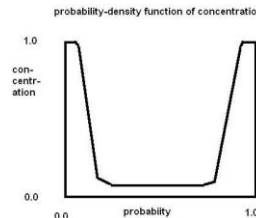
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Boussinesq's enlarged-viscosity concept predicts **macro-mixing** well, but not **micro-mixing**. It is **eddy roll-up**, enlarging interface **areas** and concentration **gradients**, which allows **laminar diffusion** to do its work.

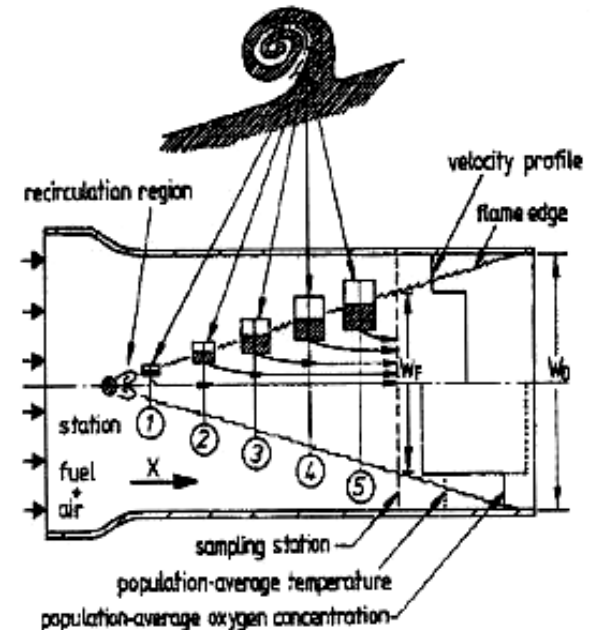


On the left is Urban Svenson's 1998 numerical simulation of the **Kelvin-Helmholtz** instability which causes eddy roll-up

The **probability-density function** for this **location** will look like **this**:



On the right is a sketch of the 1970's 'ESCIMO' concept of how 'Engulfment' and 'Stretching' increase gradients of temperature and concentration and so facilitate chemical reaction (Noseir, 1980).





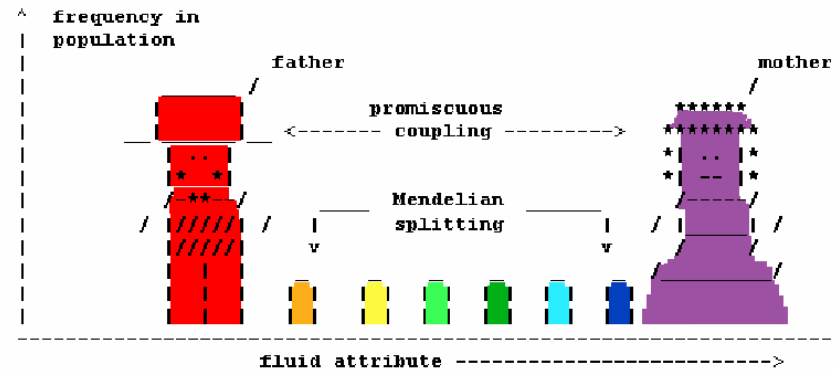
Population models of turbulent heat and mass transfer; fundamental concepts

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- In what follows, **transient engulfment** and **stretching** processes are postulated as occurring **continually and throughout** the turbulent fluid.

- They can be likened to ‘**brief encounters**’ between unlike parents, leading to offspring of **intermediate complexion**, as illustrated here:



- In the absence of other guidance, the **rate of offspring production** is taken as proportional to the **parent-concentration product**, times:
*the square root of the sum of products of **velocity gradients**.*
- This square root, multiplied by the effective viscosity, represents the **generation rate of turbulent kinetic energy**, linking conveniently with hydrodynamic turbulence models e.g. **k-epsilon**.
- The **pdf's** (now also called **population distribution functions**) of **complexion** are then computed *via* simple **mass balances**.

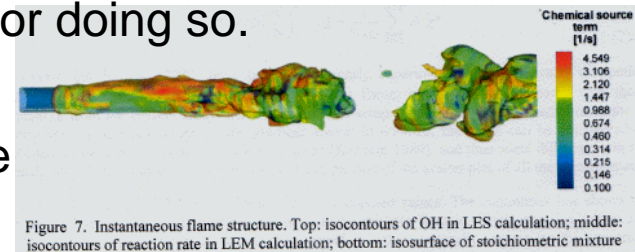


Population models of turbulent heat and mass transfer; some history

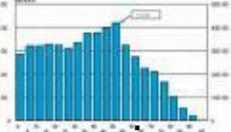
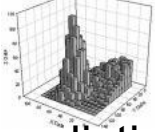
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- The use of mass-balance (*i.e.* 'pdf-transport') equations for computing population distributions was proposed by **Dopazo** in 1975.
- Numerical solutions were first provided in 1981 by **Pope**, who (wisely?) chose the **Monte-Carlo** method for doing so.
- Computations by **Fueyo** (2008) for hydrocarbon combustion, shown here, were also obtained by the Monte-Carlo method.



- In 1996, independently and as a generalisation of the 1971 '**eddy-break-up**' concept, I created the '**multi-fluid model**'. This **discretized the pdf**, treating the histogram **ordinates** as the dependent variables of a sufficient number of differential equations.

- Both **1D**  and **2D**  histograms were used; and attention was given to **how many** distinct 'fluids' (*i.e.* histogram ordinates) were required for accuracy.

This **population-grid-refinement** possibility, not available in the Monte Carlo method, is an advantage of the discretized approach.



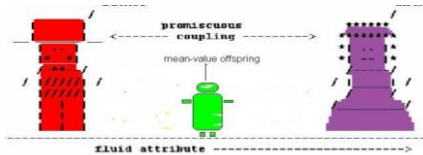
Population models of turbulent heat and mass transfer; **questions** which **research** could answer.

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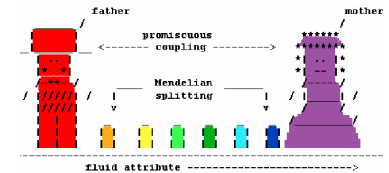
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1. The '**offspring-production-rate**' equation contains a proportionality constant (**CONMIX** below) which must be obtained from **experiment**.
 - What is its **value**?
 - **Is it** indeed a constant?
 - If not, does it depend on **Reynolds Number**? on **energy-dissipation/production-rate ratio**? on **something else**?

2. Are 'complexions' of the offspring **distributed** in uniform '**Mendelian**' fashion shown on the right)?



Or is there just one offspring complexion, as shown on the left?



3. Pdf's of temperature are **easy to measure**; and their **shapes** depend on the assumptions made for CONMIX and offspring distributions. Therefore the research questions can be answered, by **comparing** with experimental contour and pdf shapes and sizes (see next slides).

4. Unfortunately few researchers practise **both** experimental and numerical studies. How to change that is the **most pressing research challenge**.



Population models of turbulent
heat and mass transfer;
numerical solutions of the conservation equations

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Results will be presented for the much-studied steady **axi-symmetrical uniform-density turbulent jet**.

The **macro-mixing** part of the model is **conventional** in that:

- the **k-epsilon model** is employed for the calculation of the **effective viscosity**; and
- a constant **effective Prandtl number** characterises the turbulent diffusion of each of the hypothetically distinct fluids.

The **micro-mixing** part of the model is **unconventional**, in that:

- each equation has a **source term** which expresses its rate of creation by the evening out of the steep concentration gradients within the engulfed eddy; and
- it has a corresponding **sink term** expressing its contributions, with partnering 'parents', to new engulfments.

If this mingling of disparate elements is adjudged inconsistent, so be it.
Consistency is not always a virtue.

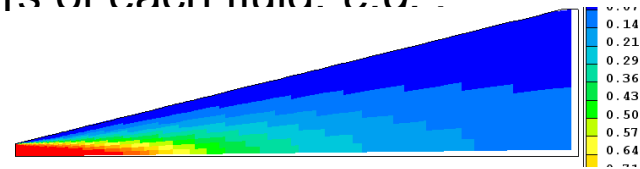


Population models of turbulence;
fluid-concentration contours for a **steady
axi-symmetrical jet** with CONMIX=100

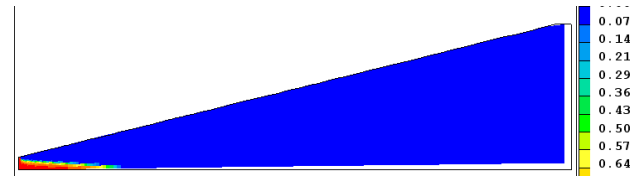
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Numerical simulation with a **20-fluid model** and a 20*100 spatial grid leads to concentration contours of each fluid. e.g. :

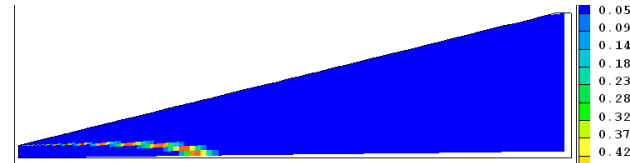
1. Sum of all 20 fluids, *i.e.* the conventional mixture fraction



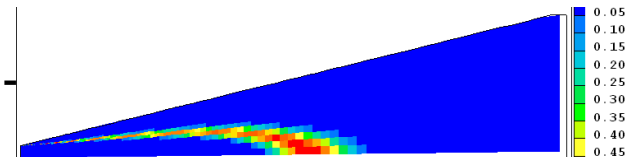
2. Fluid 1, of highest injected-substance concentration



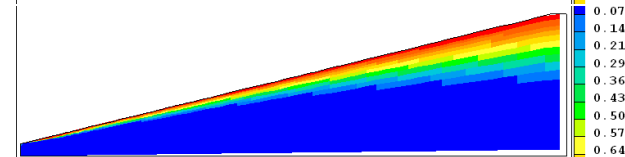
3. Fluid 10, of smaller injected-substance concentration



4. Fluid 15, of still smaller injected-substance concentration



5. Fluid 20, of smallest injected-substance concentration



Note that 20 additional differential equations had to be solved!



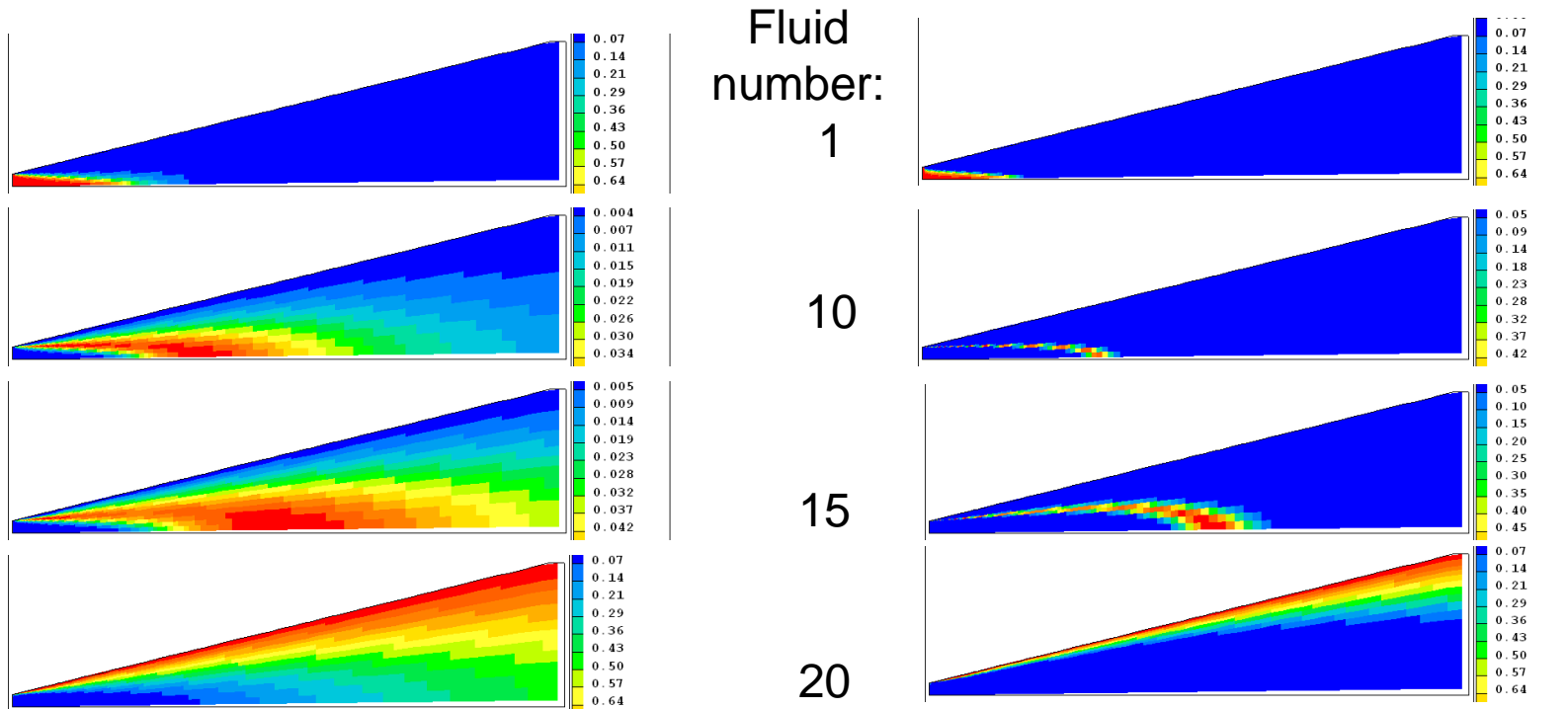
Population models of turbulence; fluid-concentration contours for the jet, with **CONMIX=1** and **100** compared

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With **CONMIX=1** (on the left) the contours are **much broader** than with **CONMIX=100** (on the right, as just seen). Which are the **more realistic**?

The **'true'** value of **CONMIX** can be established by **comparison** of experimentally-measured **pdf's** with calculated ones (see next slide).





Population models of turbulence; pdf's at two points on the jet axis, for CONMIX=1, 10 and 100

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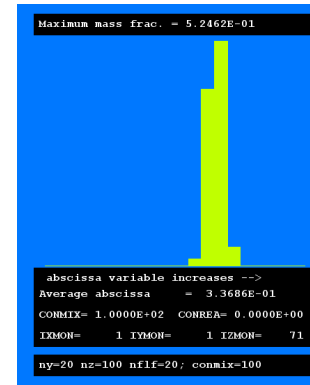
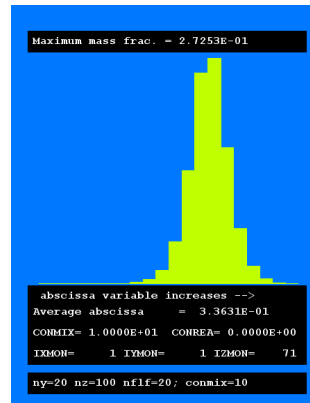
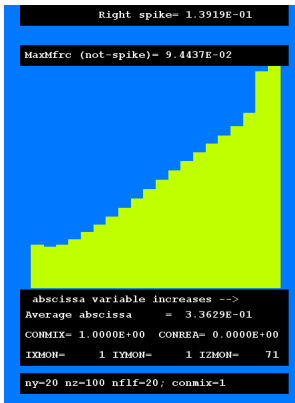
Computed pdf's for CONMIX =

1.0

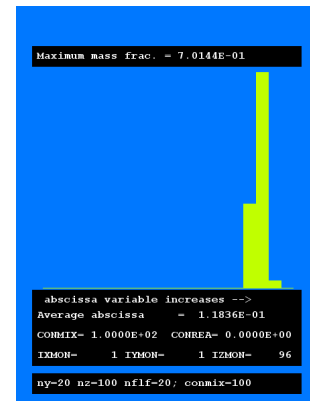
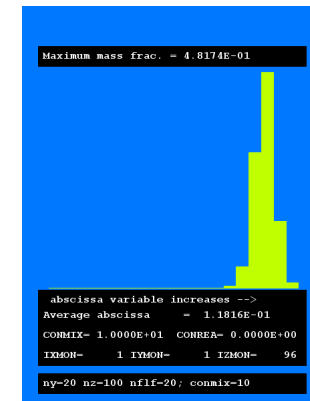
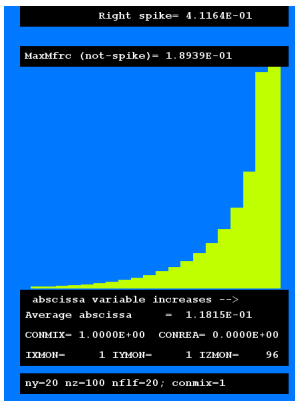
10.0

and

100.0



Axial distance
nozzle
diameter = 10



Axial distance
nozzle
diameter = 18

Such large shape differences should make it easy to determine CONMIX



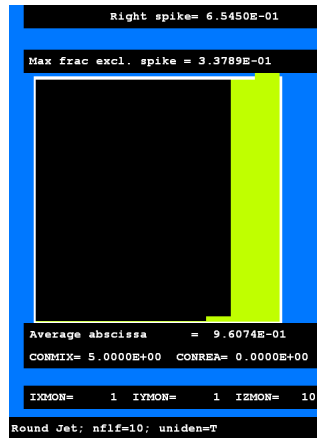
Population models of turbulent heat and mass transfer; population-grid-refinement effects

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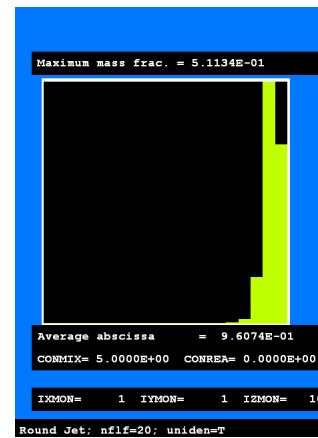
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Perhaps the 20-fluid model gives **insufficient resolution** of the pdf; therefore it is instructive to **vary the 'population-grid' fineness**, as shown below, for CONMIX= 5, for a point on the axis far from the nozzle.

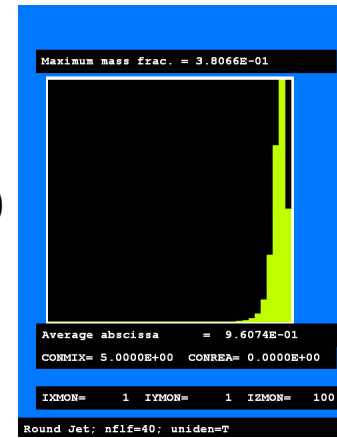
Number
of fluids
= 10



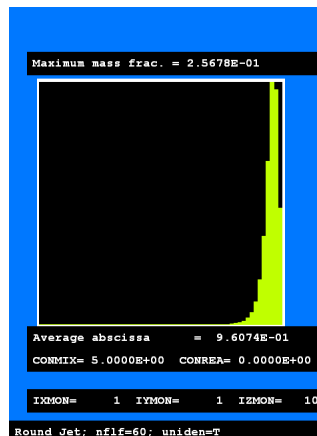
= 20



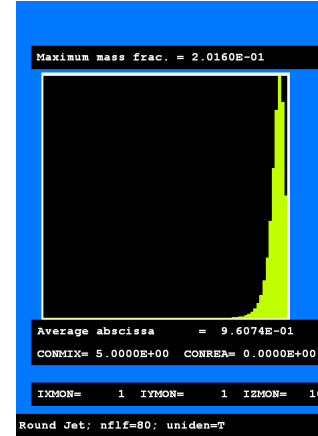
= 40



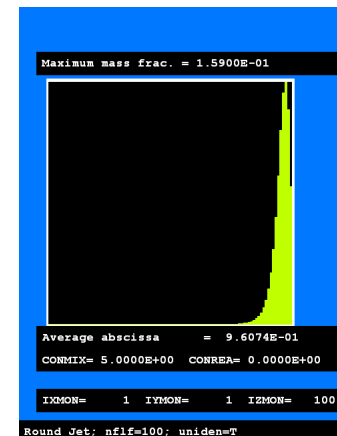
Number
of fluids
= 60



= 80



= 100





Population models of turbulent
heat and mass transfer;
comments on the foregoing results

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1. Increasing the number of fluids does give the **expected smoothing** of the pdf shape; and it of course increases the computer time also.
2. Computer times are however very **small** (less than 1 PC minute).
3. The program was PHOENICS, which has a **built-in** (but user-adjustable) **multi-fluid model** and a library of input files.
4. What is now needed is that **experimental researchers** should **use it**, or some equivalent software.
5. It is also desirable that **Direct Numerical Simulation** (DNS) practitioners should **post-process their results in terms of pdf's** and of the quantitative conditions which influence them.
6. Aiding turbulence modellers in this way may be regarded as **the main useful result** which can emerge from DNS studies, until computing power increases greatly.
7. But the modellers need to **abandon conventional Kolmogorov-type models and "think pdf"**.



Population models of turbulent
heat and mass transfer;
three **practical reasons** for **computing pdf's**

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1. Death can be caused by breathing **occasional whiffs** of high-concentration poison-gas, the **time-average** concentration of which may be **non-lethal**.



2. It is the occasional **high-velocity gust** which damages the wind turbine, **not the time-average** wind force.

3. **Explosions** can still occur when **only some** pockets of mixture are **in the flammable range** of air-fuel ratios, even though the mixture as a whole is **too rich** or **too lean** to burn.



It is differences from the mean which count !



Population models of turbulent
heat and mass transfer;
final remarks

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Four **common misconceptions** have been challenged, namely:

1. That turbulence models **must be** of **Kolmogorov** type, concerned only with **mixture-average** quantities, e.g. k , epsilon, RMS fluctuations, *etc.*, perhaps with **presumed pdf shapes**.

In fact, the pdfs of any fluid attribute (or pair of attributes) can be computed directly, with few and **testable** assumptions.

2. That Monte-Carlo methods **must be** used for computing pdfs.

In fact, **discretization** is simpler (to understand and to program), and more informative; moreover it allows population-grid refinement studies.

3. That CFD has **at most 4** dimensions (3 of space and 1 of time).

In fact, it must become **multi-dimensional** if the **population-related** aspects of fluids are to be simulated

4. That turbulence modelling is a **unique activity**, unlike any other.

In fact, it is just one branch of **population modelling**, of which other branches concern: particle-size variation, bacterial growth and decay, animal-species interaction, *etcetera*.



Population models of turbulent heat and mass transfer

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Thank you for your attention!



The End